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(54) Manufacture of bread crumblike product

(57) Farinaceous product particles having properties comparable to those of bread crumbs are formed by continuously mixing the components with gaseous leavening agent in a plug flow mixer, extruding dough from the mixer through a plurality of openings; cutting the extruded dough into particles, heating the dough particles to surface dry the particles and stabilize the shape; and subsequently drying them to the desired moisture level. The dried particles are comminuted to the desired crumb size.

ERRATUM

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Front page, Heading (72) inventors below Inventors delete whole lines insert David Victor Dyson, Michael Anthony Fourdrinier Fenn, Kenneth Stephen Darley

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	Manufacture of bread crumb-like product	
5	The present invention relates to the manufacture of a particulated leavened farinaceous product which resembles stale bread crumbs in appearance and properties. Bread particles, in the form of crumbs, are used in a variety of food products, for example, fish coatings, chicken coatings, onion rings, meat patties, and as garnishes. The bread particles	5
10	are generally produced by baking bread according to conventional yeast leavening procedures, allowing the bread to stale and then comminuting the stale loaf to the desired particle size. The time required for staling is normally about 1 to 3 days, necessitating a large storage space for the loaves while staling occurs, and the rehandling of the same, with interrupted unit processes	10
15	It has previously been suggested to utilize added gaseous materials, such as, carbon dioxide, for the leavening of bread in place of yeast leavening. The use of continuous mixers in combination with added gaseous materials also has been described, for example, in U.S. Patent and 2 041 176 to Baker. In the latter patent, flour and water are premixed to form a slurry, the	15
20	slurry is transferred by a supply hopper and a pump to a continuous mixer to which gas is introduced to form a continuous dough. The introduced gas is said by this patent to be used to raise the dough in subsequent baking to avoid the use of any yeast or ferment. While the latter procedure is useful in decreasing substantially the overall baking time for a bread product, as compared to conventional procedures, the premixing of the components to form a slurry is time consuming, the total exclusion of yeast or other ferments prevents the use	20
25	of the flavour enhancing properties thereof, and the procedure requires a baking step. The present invention provides an improved procedure for the manufacture of a particulated leavened farinaceous product of characteristics comparable to those of conventional stale bread particles, which enables such particulated farinaceous product to be produced on a continuous basis without the necessity of a baking step.	25
30	In accordance with the present invention, there is provided a continuous process for the manufacture of a particulated leavened farinaceous product, which comprises intimately mixing farinaceous product-forming components including flour and water with each other and with at least one gaseous leavening agent in a continuous mixing zone while causing partial gelation of	30
35	starch material in the farinaceous product-forming components, extruding dough from the continuous mixing zone through a plurality of openings, cutting the extruded dough into discrete dough particles, surface drying the discrete dough particles to stabilize the physical form thereof, and drying the surface-dried particles to a desired moisture level. The overall procedure involves only a short period of time, when compared to conventional	35
40	baking processes and staling procedures. The particles of leavened farinaceous product which are produced in this invention have certain characteristics which render them desirable for a variety of end uses. The particles may have any desired particle size and usually characteristic of bread crumbs. The particles may have any desired particle size and usually characteristic of bread crumbs. The particles have a stable	40
45	integral coherent shape and an opaque appearance resulting from the partially retrograded nature of the starch, are friable, and have a density of about 19 to about 35 lb/cu.ft. resulting from the porosity of the particles and to some extent, the size of the individual particles, a water absorption capability of about 1.5 to about 4 times its own weight, and a shear value of about	45
50	1.3 to about 8 kg. The initial farinaceous product-forming ingredients used in the process may comprise any of the components conventionally used in bread making and itemized under the Standards of Identity, FDA Regulations (U.S.A.) 21 C.F.R. 136.110 to .180 inclusive. The basic components of any dough are flour and water, the term "flour" including farinaceous flours used alone or in combination with other flours and meals, such as, the permitted materials outlined in 21 C.F.R.	50
55	137.105 to .350 inclusive, as well as those of legumes, rye, sorghum and rice. Varying quantities of components may be used, usually including shortening and salt in varying proportions, depending on the characteristics desired in the product and the flour used. Other farinaceous product-forming components which may be used include sugar, and oxidizing, maturing and improving agents, such as, potassium bromate, azodicarbonamide, cysteine	55
60	hydrochloride and ascorbic acid. Yeast and amylolytic or proteolytic enzymes also may be included, to modify texture and flavour in the product, as described in more detail below. Emulsifiers and cell-wall improvers	60

Yeast is conveniently used for leavening purposes in bread-making. In this invention, yeast may be used, as a flavour enhancer for the farinaceous product rather than for leavening purposes, leavening in this invention being achieved by the use of gaseous materials, such as,

65 carbon dioxide, nitrogen, air, or mixtures of gases.

	_	depend on the propert	e, the various proportions of the farinaceous product-forming ingredients ies desired, the flour used and also on the nature and choice of the able composition of ingredients, exclusive of water, which is utilized, in mix, includes:	-	
	5	Wheat flour Shortening Salt	100 parts by weight up to about 8% by weight of flour up to about 5% by weight of flour	5	
•	10	Another suitable cor mixture of flours, may	mposition of ingredients also used as a dry mix in this invention, utilizing a comprise:	10	
	15	Wheat flour Rye flour Shortening Salt	75 parts by weight 25 parts by weight up to about 8% by weight of total flour up to about 4% by weight of total	15	
		A Per	flour		
2		weight of flour:	re of the following optional components may be present, based on the	20	
2	25	Yeast Sugar Yeast food	O to about 4% by weight O to about 6% by weight O.2 to about 0.35% by weight, when yeast is present	25	
		Protease	0 to about 85,000 H.U. per 100 lb. flour		
3	30	Amylolytic enzyme	O to about 6,000 SKB units/100 lb. flour	30	•
		Mono and/or diglycerides Hydrolyzed	0 to about 5% by weight 0 to about 5% by weight		•
3		wheat starch "Tween" Surfactant	0 to about 0.75% by weight	35	ŧ
4	10	flavour. Such premixes Preferred flavour-enl	nd/or texture-modifying premixes may be used to control the product sare formed from the above optional components. Chancing mixes for use in this embodiment of the invention may be formed lurry comprising, based on the weight of total flour:	40	5
		Yeast	about 1.5 to about by% by weight about 0.05 to about 0.5% by weight		
4	45	Sugar Water	about 0.05 to about 0.5% by weight	45	
			as an additive to the other farinaceous product-forming materials. y be used to provide texture modifications to the end product. In this		ť
Ę			ed with a liquid enzyme mixture comprising, based on the weight of total	50	Š
		Amylolytic enzyme	about 1250 to about 6000 SKB		-
	55	Proteolytic enzyme	Units/100 lb. flour, and/or about 25,000 to about 85,000 H.U./ 100lb. of flour	e e	
•	,,,	Yeast food Sugar Water	about 0.25 to about 0.32% by weight about 1 to about 5% by weight about 30 to about 35% by weight	55	
6	30	Flour	about 5 to about 20% by weight	60	
		about 90 minutes.	ermented at a temperature of about 75°F to about 105°F for about 30 to		
6	35		sed in this embodiment in association with such additional water as may the desired overall moisture content and with a dry mix comprising, by	65	

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	Flour	about 80 to about 95% by weight about 1.0 to about 7% by weight	
	Salt	up to about 8% by weight	
5	Shortening		5
5	The presence of in s	situ salt in crumbs is advantageous in certain end uses and high levels of	
10	salt are attainable in the leavening. This contrast concentrations above a limiting the quantity of the process of this contrast of the process of the contrast of the contras	his invention, since high concentrations do not adversely interiere with the sts markedly with conventional bread-forming procedures wherein salt about 2% by weight decrease the leavening action of the yeast, thereby f salt which can be incorporated into the final bread crumbs. is invention, the farinaceous product-forming ingredients are fed to inlets were mixing zone capable of plug flow therethrough. The mixing zone	10
15	may take the form of a required processing co one end of the mixer in intermixed component 43% by weight. The discount of the component of the	an elongate screw-type mixer-extruder, suitably modified to provide the onditions therein. The farinaceous product-forming components are fed to in relative proportions suitable to provide an overall moisture content of its of about 30 to about 50% by weight, preferably about 37 to about dry mix, water, and any yeast slurry, are usually separately fed to the	15
20	intermixed while they	one, the farinaceous product-forming components are continuously are conveyed from one end of the mixing zone to the other, over a time about 100 seconds, preferably about 20 to about 50 seconds. d gaseous inlets is provided along the length of the mixing zone and a	20
25	gaseous material, or m Carbon dioxide usually although other materia zone is in the range of	nixture of gaseous materials, is injected into the mix through the openings. y is used, often in admixture with nitrogen, as the gaseous material, als may be used, including air and oxygen. The total gas fed to the mixing f about 1 to about 30 SCFH, preferably about 8 to about 12 SCFH, per	25
30	forces within the mixir components and dispe- within the mixing zone	educt-forming components and the injected gas are subjected to high shearing zone, sufficient to cause simultaneous uniform mixing of the ersion of the inert gas throughout the mix. The work is done on the dough e varies from about 15 to about 40 watt hr/lb of dough, preferably about	30
35	20 to about 30 watth The mix of farinaced zone for at least a maj cause partial gelation nents. The temperature	nr/lb. ous product-forming components and inert gas is heated within the mixing jor proportion, typically about 75%, of the length of the mixing zone to of starch material contained in the farinaceous product-forming compore in the mixing zone is maintained sufficiently high that the heat applied esulting from the high shear mixing results in a dough emerging from the temperature of about 90° to about 210°F, preferably about 130° to about	35
40	170°F, to achieve the The dough resluting back pressure which is	e partial gelation. If the partial gelation is the mixing zone is extruded therefrom under a gradually in the range of about 200 to about 600 psig, and is preferably in the partial achieved by suitable design of the extrusion die.	40
45	The operations effect product will have the	properties of stale bread crumbs and no holding time is required at any	45
	In this invention, the farinaceous product-for zone while leavening to water and gas are tho	nerefore, the flour and water are separately fed directly to the mixer, the common components are conveyed in plug flow manner through the mixing gas is injected into the mix at a plurality of spaced locations, the flour, proughly intermixed under critical high shear, temperature and back and the dough-forming process is rapidly completed.	50
	In a preferred embo direct control to be ex slurry added directly t	rediment of the present invention, the very short overall mixing time permits recised over the flavour of the final product, by the use of a yeast-based to the mixer at the upstream end.	55
55	on leaving the mixer. number of orifices three rectangular and about	Exit from the mixer is accomplished through a die containing a suitable rough which the dough passes. The cross-section of the orifices is usually to about 1" in dimension but may be of any other desired geometry the face of the die to produce dough pieces between about 1/16 and less, preferably between about 1/16 and about 3/16 inch and preferably	
60	about 1/2 to about 3 The dough pieces a pressure lift. The air li	3/4" in cross-section. are transported to a conventicanal forced air dryer using a hot air suction of ift temperature ranges from about 180 to about 300°F preferably about to the hot air in the lift assists drying by preheating the dough pieces and	60
65	a continue accordance descina	g enabling the pieces to remain as discrete particles on the drier bed. It there is a tendency for the particles to agglomerate and form a solid	65

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sheet on the dryer bed which hinders air flow.

After drying to the desired moisture, usually less than about 10 wt.%, the dough pieces are comminuted to a suitable size for use, usually less than about 5 mm.

The invention is illustrated by the following examples:

Example 1

An initial dry mix containing the following ingredients was prepared:

	Component	% by weight	
10	Hard wheat flour	47.853	10
	Rapido 80*	23.926	. •
	Pastry flour	23.926	
	Shortening	2.871	
	Seasoning	1.424	
15	_		15
		100.00	

Rapido 80 is a commercially available bread flour.

The dry mix was fed into one end of the extruder at 4.7 kg/min. Water was added to the 20 same end of the extruder at 1.03 kg/min., 31% of which was added in a preconditioning screw 20 and the remaining 69% at the start of the extruder. In addition a yeast brew consisting of:

	Yeast	5.44 k		
	Water	60	kg	
25	Dextrose	1	kg	

was metered in at the one end of the extruder at a rate of 1 litre/min. to give a total moisture content of 39%.

The components were continuously intermixed during passage from one end of the extruder 30 to the other over a period of about 20 seconds. Carbon dioxide was fed into the extruder at 3 different locations at the rate of 10.5 SCFH/100 lb. dough while the extruder was heated to result in a dough temperatue of 130°F at the exit. Work was applied to the dough during formation thereof and passage through the extruder of 27 watt hr/lb and a back pressure of 300 psig existed at the outlet orifice.

35 The dough was extruded through rectangular openings dimensioned 5/8 × 7/8 inch and cut into particles of length of 3/16 inch. These particles were conveyed by means of an upflow of hot air at a temperature of 280°F for about 3 seconds to surface dry the wet particles. The surface dried non-sticky dough particles were then dried by conventional hot air drying at a temperature of about 300°F to a moisture content of less than about 10 wt.%.

40 The dried dough particles had the properties set forth in the following Table I:

TABLE I

Bulk density 22.5 lb/ft³

Absorption 3.43 × own weight

45 Shear 3.10 kg 45

Example 2

An initial dry mix containing the following ingredients was prepared:

50	An initial dry iniz	containing the lo	nowing ingi	edients	was prepare	u.	50
	Component	% by weight					
	Pastry flour	71.0					
	Hard wheat flour	23.25					
	Shortening	3.0					
55	Salt	2.5					55
	Atmul 500*	0.25					
		100.00			•		
		100.00					

60 * A mixture of mono- and di-glycerides sold by Atlas Chemical Company.

The dry mix was fed into the one end of the extruder at 6.6 kg/min. Water was added at the same end at 2.78 litres/min; 10% of which was added in the preconditioning screw and the remaining 90% at the start of the extruder, to provide a moisture content of 39 wt.%.

The components were continuously intermixed during passage from one end of the extruder to the other over a period of about 20 seconds. Carbon dioxide was fed into the extruder at

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5	three locations under 150 psi pressure at a rate of 4.3 SCFH/100 lb. of dough. The extruder was heated to give a dough exit temperature of 150°F. Work was applied to the dough during formation thereof and passage through the extruder of 21 watt hr/lb. and a back pressure of 300 psig existed at the outlet orifice. The dough was extruded through rectangular openings of diameter 5/8 × 7/8 inch and cut into particles of length 1/8 inch. These particles were conveyed by means of a flow of hot air at	5
	a temperature of 280°F for about 3 seconds to surface dry wet particles. The surface-dried non-sticky dough particles were then dried by conventional hot air drying at about 300°F to a final moisture of less than about 10 wt.%.	10
10	The dried dough particles had the properties set forth in the following Table II:	10
	TABLE II Bulk density 25 lb/ft³ Absorption 3.1 × own weight	15
15	In summary of this disclosure, the present invention provides a unique procedure for the preparation of comminuted farinaceous product having properties comparable to stale bread particles which involves only a very short overall period of time. Modifications are possible within the scope of the invention.	
20		20
25	CLAIMS 1. A continuous process for the manufacture of a particulated leavened farinaceous product, which comprises intimately mixing farinaceous product-ferming components including flour and water with each other and with at least one gaseous leavening agent in a continuous mixing zone while causing partial gelation of starch material in said farinaceous product-forming components, extruding dough from the continuous mixing zone through a plurality of openings and cutting the extruded dough into discrete dough particles, surface drying the discrete dough particles, surface drying the discrete dough particles to stabilize the physical form thereof, and	25
30	drying the surface-dried particles to a desired moisture level. 2. A process as claimed in claim 1 in which the farinaceous product-forming components are fed to the continuous mixing zone in quantities to provide a total moisture content of 30 to 50%	30
35	by weight. 3. A process as claimed in claim 2 in which the moisture content is 37 to 43 wt.%. 4. A process as claimed in any one of claims 1 to 3, in which the farinaceous product- forming components are advanced in plug flow manner through the mixing zone in 15 to 100 seconds.	35
	5. A process as claimed in claim 3, in which the components are advanced throught the	
40	mixing zone in 20 to 50 seconds. 6. A process as claimed in any one of claims 1 to 5, in which the gaseous leavening agent is introduced to the farinaceous product-forming components at a plurality of locations during passage of the components through the mixing zone at a gas flow rate of 1 to 30 SCFH/100 lb of farinaceous product-forming components.	40
	7. A process as claimed in claim 6, in which the gas flow rate is 8 to 12 SCFH/100 lb of farinaceous product-forming components.	
45	the state of the s	45
50	components and distribution of gaseous material within the mixture. 9. A process as claimed in claim 8, in which the work applied is 20 to 30 watt hr/lb of foreigneous product-forming components.	50
55	10. A process as claimed in any one of claims 1 to 9 in which the partial gelation of the startch material is achieved by subjecting the farinaceous product-forming components and introduced gaseous material to an elevated temperature within the mixing zone during at least a major proportion of the time of passage through the mixing zone. 11. A process as claimed in any one of claims 1 to 10, in which the extruded dough has a	55
60	temperature of 90° to 210°F. 12. A process as claimed in claim 11, in which the dough temperature is 130° to 170°F. 13. A process as claimed in any one of claims 1 to 12, in which the farinaceous product- forming components are subjected to a back pressure of 200 to 600 psig. 14. A process as claimed in claim 13, in which the back pressure is 250 to 400 psig. 15. A process as claimed in any one of claims 1 to 14, in which the dough is extruded from	60
65	the mixing zone through a die having a plurality of openings therein having a maximum diameter of $\frac{1}{2}$ to 1 inch and the dough extruded through the plurality of openings is cut into discrete dough particles of $1/16$ to $\frac{1}{2}$ inch in length.	65

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5	have a dimension of 17. A process as dough particles is effective 18. A process as 230° to 290°F.	claimed in claim 17, in which the flowing air stream has a temperature of	5
10	are dried to a moistur 20. A process as agent comprises carbo	claimed in any one of claims 1 to 18, in which the surface-dried particles be level of below 10% by weight. claimed in any one of claims 1 to 19, in which the gaseous leavening on dioxide. claimed in any one of claims 1 to 20, in which the farinaceous product-	10
15	forming components in 22. A process as	include salt in a concentration of up to about 7% by weight of flour. claimed in any one of claims 1 to 21, in which the farinaceous product-exclusive of water, comprises:	15
20	Flour Shortening Salt	100 parts by weight up to 8% by weight of flour up to 5% by weight of flour	20
20		claimed in any one of claims 1 to 21, in which the farinaceous product- exclusive of water, comprise:	20
25	Wheat flour Rye flour Shortening Salt	75 parts by weight 25 parts by weight up to 8% by weight of total flour up to 4% by weight of total flour	25
30		claimed in claim 22 or 23, in which the farinaceous product-forming ontain at least one further component selected from:	30
35	Yeast Sugar Yeast food Protease Amylolytic enzyme	0 to 4% by weight 0 to 6% by weight 0.2 to 0.35% by weight when yeast is present 0 to 85,000 H.U. per 100 lb. of flour 0 to 6000 SKB units per 100 lb.	35
40	Mono and/or diglycerides	of flour 0 to 2% by weight	40
45		0 to 5% by weight 0 to 0.75% by weight claimed in claim 24, in which a flavour-enhancing premix is incorporated duct-forming components by utilizing a slurry comprising, based on the	45
50	Yeast Sugar Water	1.5 to about 3.5 by weight 0.05 to 0.5% by weight 10 to 25% by weight	50
55	26. A process as claimed in claim 25, in which the slurry is mixed with a liquid enzyme mixture, comprising, based on the total weight of flour:		
60	Amylolytic enzyme Proteolytic enzyme Yeast food Sugar Water Flour	1250 to 6000 SKB units per 100 lb. of flour, and/or 25,000 to 85000 H.U. per 100 lb. of flour 0.25 to 0.32% by weight 1 to 5% by weight 30 to 35% by weight 5 to 20% by weight	60
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and the mixture is fermented at a temperature of 75°F to 105°F for 30 to 90 minutes before incorporation in the farinaceous product-forming components.

27. A process as claimed in any one of claims 1 to 26, including comminuting the dried

particles to a desired particle size.

28. A continuous process for the manufacture of a particulated leavened farinaceous product substantially as hereinbefor described with reference to any one of the Examples.

29. Particulated farinaceous product whenever prepared by a process as claimed in any one

of claims 1 to 28.

30. Particulated farinaceous product of stable integral coherent shape, which are opaque 10 and friable, and have a density of 19 to 35 lb/cu.ft., a water absorption capability of 1.5 to 4 times its weight, and a shear value of 1.3 to 8 kg, whenever prepared by a process as claimed in any one of claims 1 to 28.

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